

(19)



Europäisches Patentamt
European Patent Office
Office européen des brevets



(11) Publication number:

0 472 693 B1

(12)

EUROPEAN PATENT SPECIFICATION(45) Date of publication of patent specification: 15.11.95 (51) Int. Cl.⁸: **C07F 9/38**(21) Application number: **91905864.4**(22) Date of filing: **12.03.91**(66) International application number:
PCT/ES91/00013(67) International publication number:
WO 91/13893 (19.09.91 91/22)

(54) **PREPARATION OF N-PHOSPHONOMETHYLGLYCIN BY OXIDATION OF
N-PHOSPHONOMETHYLIMINODIACETIC ACID.**

(30) Priority: **12.03.90 ES 9000732**(43) Date of publication of application:
04.03.92 Bulletin 92/10(45) Publication of the grant of the patent:
15.11.95 Bulletin 95/46(94) Designated Contracting States:
DE DK FR GR IT(56) References cited:
EP-A- 0 314 662
FR-A- 2 193 831

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Description**FIELD OF THE INVENTION**

5 The invention relates to improvements introduced into a method of obtaining N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid with oxygen or a gas containing oxygen, utilising as catalyst a noble metal supported on activated carbon. Specifically, the improvements of the invention relate to a treatment directed towards minimising the loss of the noble metal catalyst which occurs in this type of reaction.

ANTECEDENTS OF THE INVENTION

10 N-phosphonomethylglycine, described in the United States of America Patent 3.799.758, is a known herbicide and its use is very widespread. Since its appearance on the market, various methods for obtaining it have been described and patented. One of these methods, specifically, the one claimed in the Spanish Patent No. 415.335 in the name of the Monsanto Company (equivalent to US-A-3954848) provides a method of obtaining N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid with oxygen or a gas containing oxygen, utilising a noble metal (Pd, Pt, Rh) supported on activated carbon as catalyst for the reaction. Although this method allows for obtaining N-phosphonomethylglycine in acceptable yield and state of purity, it has the disadvantage that the losses of the noble metal used as catalyst are so great (may be as much as 30 %) that said method is not economically profitable and that the losses of the noble metal increase the price of the finished product to such an extent that the method is not viable on an industrial scale.

25 On the other hand, it is a fact known by the technical experts in catalysis that the losses of the noble metal which occur in the both acidic and basic catalytic methods, is by dissolution of said metal in the reaction water, thus requiring a complex and costly treatment to recover said metal. Consequently, this type of method is not viable in practice for obtaining finished products with slightly increased value.

30 Therefore, it would be advantageous to have available a method which allows for obtaining N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid with oxygen, in the presence of a noble metal catalyst which overcomes the disadvantages referred to previously. In particular, it would be advantageous for this method to minimise the losses of noble metal used as catalyst in such a way that they do not substantially increase the cost of the finished product, with the object of rendering this method industrially viable.

35 Consequently, an object of the invention is the introduction of improvements over the known methods of obtaining N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid with oxygen, in the presence of a noble metal supported on activated carbon as catalyst, providing that said improvements minimise the losses of noble metal, by means of implementation of a treatment intended to recover practically the total amount of the catalyst utilised, without loss of its catalytic activity.

BRIEF DESCRIPTION OF THE INVENTION

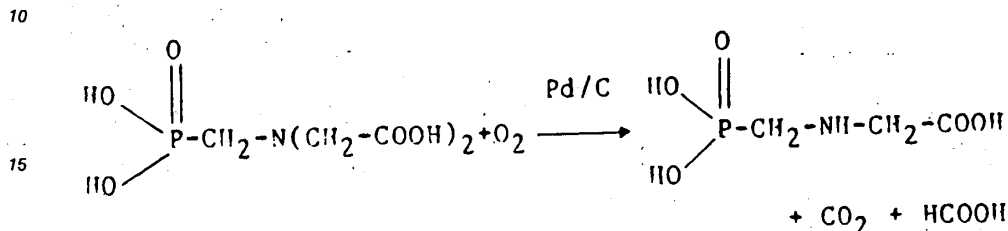
40 The improvements of the invention may be stated as specifically to minimise the losses of the noble metal catalyst used for obtaining N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid. For minimising these losses, the invention proposes effecting a flushing-out with nitrogen once the oxidation reaction is completed.

45 The present invention provides for a method for obtaining N-phosphonomethylglycine by the oxidation under pressure of N-phosphonomethyliminodiacetic acid with oxygen or a gas containing oxygen, in the that, once the reaction has been completed and before proceeding with its cooling, a flushing-out with nitrogen is carried out at a pressure between 49 and 490 kPa (between 0.5 and 5 kg/cm²) for a sufficient period of time to reduce the concentration of the noble metal in the reaction medium to less than 1 ppm. In addition, prior to the flushing-out with nitrogen under pressure, a depressurization and flushing-out with nitrogen may be effected to remove oxygen.

50 Due to this, it follows that the content of noble metal in the reaction solution is less than 1 ppm, compared with a content of said metal greater than 70 ppm which is present in said solution if the flushing-out with nitrogen is not effected. Therefore, this flushing-out with nitrogen minimises the losses, lowering the percentage loss from 30% to less than 1%, in this way making this type of method economically viable. The obtaining of these improvements will be referred to in detail in the following description.

DETAILED DESCRIPTION OF THE INVENTION

The invention provides a series of betterments or improvements directed towards minimising the losses of noble metal used as catalyst in the known method for obtaining N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid. In the prior Patent cited in the antecedents for the invention, a method for obtaining N-phosphonomethylglycine is described which may be characterised in accordance with the following equation in which, for the sake of simplicity, palladium on carbon Pd/C is used as the catalyst:



20 The reaction is carried out in the temperature range between 25°C and 125°C, preferable between 90°C and 105°C, at a pressure in the range between 1 and 5 kg/cm². However, for the reasons indicated previously, the method disclosed in said Patent is not viable on the industrial scale. In order for said method to become industrially viable, the losses of catalyst would need to be minimised.

Therefore, an economical and simple form of said method has been sought to render it industrially viable. This has resulted from making use of the improvements provided by the present invention. These improvements consist of effecting a treatment of the reaction solution once the reaction has been completed to recover practically the total amount of the catalyst utilised, without alteration of its catalytic activity and capability of being re-utilised to catalyse this type of reaction without varying the yields. Consequently, in a first phase, the oxidation of N-phosphonomethyliminodiacetic acid with oxygen or a gas containing oxygen is carried out in the presence of a noble metal catalyst supported on activated carbon and, once this reaction is completed, the reaction solution obtained is flushed-out with nitrogen under pressure for the purpose of recovering the noble metal in accordance with the method of operation to be described later.

For carrying on the oxidation reaction to completion, it has been found that it is advantageous to carry on said reaction at a temperature in the range between 100°C and 105°C, at a pressure in the range between 294 and 392 kPa (between 3 and 4 kg/cm²), using water as the solvent at a pH value in the range between 4 and 8, with the best results being obtained at a pH value close to 7.

The initial concentration of N-phosphonomethyliminodiacetic acid should be in the range between 4% and 15% by weight, preferable between 4% and 6% by weight, because higher concentrations diminish the yield from the reaction and lower concentrations diminish the productivity. The percentage of catalyst calculated with respect to the N-phosphonomethyliminodiacetic acid may be varied between 4% and 10% by weight, although with a mean percentage of 6%, it is possible to obtain very good results. For implementation of this invention, palladium on carbon (Pd/C) has been used as the catalyst.

Once the oxidation reaction has been completed, with the object of minimising the loss of the noble metal, the treatment which follows, and which constitutes the improvement provided by the present invention, is carried out. Said treatment may be summed up as being that, in a single phase after completion of the reaction in an atmosphere of oxygen, or of a gas containing oxygen, the reaction solution obtained is de-pressurised and is flushed-out twice with nitrogen, with the object of removing as much oxygen as possible from the reaction solution. Following this, the reaction vessel is re-pressurised with nitrogen, at a pressure in the range between 49 and 490 kPa (between 0.5 kg/cm² and 5 kg/cm²), preferably between 98 and 196 kPa (between 1 and 2 kg/cm²) and, maintaining this pressure, the passage of nitrogen is continued at a flow rate from 10 to 30 litres/minute, during a period of time lasting from 15 minutes up to 1 hour. Obviously, the flow rate (litres/minute) of nitrogen depends upon the scale of the process. The period of time of passing-in the nitrogen is a function of the temperature of the reaction solution, which may be between 20°C and 120°C, since the reaction mixture, when pressurised with nitrogen could heat up or, alternatively, this treatment could be carried out at the temperature of the oxidation reaction without the necessity of heating the reaction solution. It has been found that, with a temperature of the reaction solution of 115°C, the period of time for the passage of nitrogen is 30 minutes in order to obtain a content of 0.9

ppm of palladium in said solution and that, at a temperature of 100 °C, the period of time for the passage of nitrogen is 45 minutes in order to obtain a content of 0.6 ppm of palladium in said solution. When the content of palladium in the reaction solution is less than 1 ppm, determined by atomic absorption, the reaction vessel is de-pressurised, the catalyst is filtered off for later use and the filtrate obtained is concentrated in vacuo. The N-phosphonomethylglycine is obtained by re-crystallisation.

If the treatment is not carried out, then the content of palladium in the reaction solution is greater than 70 ppm, as is evident in the examples which accompany this description. These losses of noble metal greater than 70 ppm lead to an increase in cost of the finished product beyond the limits of economic viability.

However, by means of the treatment, proposed by this invention of the reaction solution once the reaction is completed, the losses of noble metal in the solution are minimised, and make viable, in a simple manner, a method which was not carried out in the procedures referred to earlier. Furthermore, the recovered catalyst maintains its catalytic activity and may be re-utilised at least for 20 consecutive times without loss of its activity and without altering the yields.

Consequently, by means of the improvements due to this invention, it is possible to obtain N-phosphonomethylglycine by oxidation of N-phosphonomethyliminodiacetic acid, at the industrial level with an adequate purity and yield and, furthermore, it is possible to recover the noble metal catalyst used, without loss of its catalytic activity by means of a simple treatment which does not require the installation of complex equipment.

The present invention will be clearly illustrated with the following examples.

EXAMPLE 1

In a stainless-steel (AISI 316) autoclave reactor of 40 litres capacity, there are introduced in the following order: 2.045 Kg of N-phosphonomethyliminodiacetic acid of 97% purity, 33.974 Kg of water at a pH value of ca. 7, and 121.5 grams of dry catalyst (commercial) of 5% palladium on carbon, which represents 6.075 grams of pure palladium by assay.

Following this, the passing in of oxygen is continued until an internal pressure of 353-373 kPa (3.6 - 3.8 kg/cm²) is reached and the mixture heats up, maintaining the given pressure until a temperature of 100 °C is reached, having oxygen passed through the mixture at a flow rate of 2.5 litres/minute. The suspension is stirred continuously under these conditions for a period of 2 hours. When the stated period of time has elapsed, a sample is taken and, after the catalyst has been removed by filtration, is analysed for the content of N-phosphonomethyliminodiacetic and the ppm of palladium present, finding 110 ppm. When it is confirmed that at least 95 of the starting material has been converted, the supply of oxygen is cut off and the reactor is de-pressurised, changing over to pressurisation this time with nitrogen up to a pressure of 196 kPa (2 kg/cm²) and the reaction solution is heated to 115 °C, maintaining this condition with bubbles of nitrogen through the reaction mixture at a flow rate of 24 litres/minute during a period of time of at least 30 minutes. When the treatment is completed and it has been shown that the reaction solution at this moment has a palladium content of less than 1 ppm (0.9 ppm), the preceding treatment is terminated and the reactor is depressurised, the catalyst is filtered off and the filtrate obtained is later concentrated in vacuo and the N-phosphonomethylglycine is obtained by re-crystallisation. The yield of N-phosphonomethylglycine having a degree of purity greater than 97 % was 1.449 kg (yield 96.4%).

EXAMPLE 2.

This experiment was carried out to determine the influence of temperature on the process of recovery of the palladium dissolved in the reaction solution. The experiment was carried out with the same method utilised for the reaction in Example 1. With regard to the treatment after the reaction for recovery of the palladium, this was carried out at a temperature equal to that of the reaction (100 °C) and the time employed so that the dissolved palladium was less than 1 ppm (0.6 ppm) in the reaction water was 45 minutes.

The yield of N-phosphonomethylglycine having a degree of purity greater than 97% was 1.440 kg (yield 95.6%).

Claims

1. A method for obtaining N-phosphonomethylglycine by the oxidation under pressure of N-phosphonomethyliminodiacetic acid with oxygen or a gas containing oxygen, in the presence of a

catalyst of noble metal supported on activated carbon, characterised in that, once the reaction has been completed and before proceeding with its cooling, a flushing-out with nitrogen is carried out at a pressure between 49 and 490 kPa (between 0.5 and 5 kg/cm²) for a sufficient period of time to reduce the concentration of the noble metal in the reaction medium to less than 1 ppm.

- 5 2. The method of claim 1 characterized in that, prior to the flushing-out with nitrogen under pressure, a depressurization and flushing-out with nitrogen is carried out to remove oxygen.
3. The method of Claim 1 or 2 characterized in that, the flushing-out with nitrogen is effected at a
10 temperature in the range between 20 °C and 120 °C.
4. The method according to Claim 1 or 2, characterized in that the passing-in of nitrogen is carried on for a period of time lasting from 15 minutes up to 1 hour.
- 15 5. The method according to any preceding claim, characterized in that the noble metal is palladium.

Patentansprüche

- 20 1. Verfahren zur Herstellung von N-Phosphonomethylglycin durch die Oxidation von N-Phosphonomethyliminodiessigsäure unter Druck mit Sauerstoff oder einem Sauerstoff enthaltenden Gas in Gegenwart eines Katalysators aus Edelmetall, welches auf Aktivkohle als Träger vorliegt, **dadurch gekennzeichnet**, daß, nachdem die Umsetzung beendet ist und bevor dem mit deren Kühlung fortgefahren wird, eine Ausspülung mit Stickstoff bei einem Druck zwischen 49 und 490 kPa (zwischen 0,5 und 5 kg/cm²) während eines ausreichenden Zeitraums durchgeführt wird, um die Konzentration des Edelmetalls in
25 dem Reaktionsmedium auf weniger als 1 ppm zu vermindern.
2. Verfahren nach Anspruch 1, **dadurch gekennzeichnet**, daß vor dem Ausspülen mit Stickstoff unter Druck, ein Druckabbau und ein Ausspülen mit Stickstoff durchgeführt wird, um Sauerstoff zu entfernen.
- 30 3. Verfahren nach Anspruch 1 oder 2, **dadurch gekennzeichnet**, daß das Ausspülen mit Stickstoff bei einer Temperatur im Bereich zwischen 20 °C und 120 °C bewirkt wird.
4. Verfahren nach Anspruch 1 oder 2, **dadurch gekennzeichnet**, daß das Einleiten von Stickstoff während eines Zeitraums von 15 Minuten bis 1 Stunde weitergeführt wird.
- 35 5. Verfahren nach mindestens einem der vorangehenden Ansprüche, **dadurch gekennzeichnet**, daß das Edelmetall Palladium ist.

Revendications

- 40 1. Procédé pour obtenir la N-phosphonométhylglycine par oxydation sous pression de l'acide N-phosphonométhyliminodiacétique avec de l'oxygène ou un gaz contenant de l'oxygène, en présence d'un catalyseur de métal noble supporté sur du charbon actif, caractérisé en ce que, dès que la réaction a été achevée et avant de procéder à son refroidissement, un rinçage à l'azote est exécuté à une
45 pression comprise entre 49 et 490 kPa (entre 0,5 et 5 kg/cm²) pendant une durée suffisante pour réduire la concentration du métal noble dans le milieu réactionnel à moins de 1 ppm.
2. Procédé selon la revendication 1, caractérisé en ce que, avant le rinçage à l'azote sous pression, une dépressurisation et un rinçage à l'azote sont exécutés pour éliminer l'oxygène.
- 50 3. Procédé selon la revendication 1 ou 2, caractérisé en ce que le rinçage à l'azote est effectué à une température comprise dans la gamme 20 °C-120 °C.
4. Procédé selon la revendication 1 ou 2, caractérisé en ce que le passage de l'azote est effectué pendant une durée de 15 minutes jusqu'à 1 heure.
- 55 5. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que le métal noble est le palladium.

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